PATENT COOPERATION TREATY

PCT

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

(Chapter II of the Patent Cooperation Treaty)

(PCT Article 36 and Rule 70)

REC'D 2 7 JUN 2005

Applicant's of agent's file reference				
Cal 88473	FOR FURTHER ACTION	See Form PCT/IPEA/416		
International application No.	International filing date (day/month/year)	Priority date (day/month/year)		
PCT/EP2004/009684	31.08.2004	04.09.2003		
International Patent Classification (IPC) or national classification and IPC				
C08J11/08, C08J3/09				
Applicant				
POLIMERI EUROPA S.P.A.				
This report is the international prelin Authority under Article 35 and trans	minary examination report, established smitted to the applicant according to Arti	by this International Preliminary Examining		
2. This REPORT consists of a total of 4 sheets, including this cover sheet.				
This report is also accompanied by	ANNEXES, comprising:			
a. 🖾 sent to the applicant and to	the International Bureau) a total of 6 sl	heets as follows:		
I Sheets of the description	Claime and by drawings			
and/or sheets containing Administrative Instructio	rectifications authorized by this Author	een amended and are the basis of this report rity (see Rule 70.16 and Section 607 of the		
☐ sheets which supersede	A Carlior chapte had added to the			
beyond the disclosure in	the international application as filed, a	considers contain an amendment that goes indicated in item 4 of Box No. I and the		
sequence listing and/or table	reau only) a total of (indicate type and n	number of electronic carrier(s)) , containing a		
Box Relating to Sequence L	isting (see Section 802 of the Administr	number of electronic carrier(s)) , containing a storm only, as indicated in the Supplemental rative instructions.		
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This report contains Indications rela	ting to the following items:			
☐ Box No. I Basis of the opinion	on			
☐ Box No. II Priority				
☐ Box No. III Non-establishmer	nt of opinion with regard to novelty, inve	ntivo eten and today to the		
☐ Box No. IV Lack of unity of in	vention	milve step and industrial applicability		
Box No. V Reasoned statem	ent under Article 25(0) with manual to	Ovelty, inventive step or industrial		
	and exhibitiations supporting such s	statement		
= zextre. it Gertain document				
	the international application			
☐ Box No. VIII Certain observation	ns on the international application			
Date of submission of the demand	I Date of			
	Date of completion	of this report		
31.03.2005				
	27.06.2005			
Name and mailing address of the international	Authorized Offi			
preliminary examining authority:				
European Patent Office - P.B. 5818 Patentlaan 2 NL-2280 HV Rijswijk - Pays Bas Hallomoocob A				
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INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

International application No. PCT/EP2004/009684

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_		x No. I	Basis of the report .	
1.	. With regard to the language, this report is based on the international application in the language in which it if the filed, unless otherwise indicated under this item.			
		☐ inte	eport is based on translations from the original language into the following language, is the language of a translation furnished for the purposes of: ernational search (under Rules 12.3 and 23.1(b)) elication of the international application (under Rule 12.4) ernational preliminary examination (under Rules 55.2 and/or 55.3)	
2.	Wi ha rep	th regard <i>ve been</i>	It to the elements* of the international application, this report is based on <i>(replacement sheets which furnished to the receiving Office in response to an invitation under Article 14 are referred to in this priginally filed" and are not annexed to this report):</i>	
De		scription,	, Pages	
	1-2	0	as originally filed	
	Claims, Numbers			
	1-18 received on 05.04.2005 with letter of 04.04.2005			
		a seque	ence listing and/or any related table(s) - see Supplemental Box Relating to Sequence Listing	
3.		☐ the d ☐ the d ☐ the d ☐ the d	nendments have resulted in the cancellation of: description, pages claims, Nos. drawings, sheets/figs sequence listing (specify): table(s) related to sequence listing (specify):	
4.	had Sup	plementa the c the c the c the d the d	port has been established as if (some of) the amendments annexed to this report and listed below an made, since they have been considered to go beyond the disclosure as filed, as indicated in the description, pages claims, Nos. Irawings, sheets/figs requence listing (specify): stable(s) related to sequence listing (specify):	
			m 4 applies, some or all of these sheets may be marked "superseded."	

INTERNATIONAL PRELIMINARY REPORT ON PATENTABILITY

International application No. PCT/EP2004/009684

Box No. V Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

1. Statement

Novelty (N)

Yes: Claims

1-18

No: Claims

Inventive step (IS)

Yes: Claims

1-18

No: Claims

Industrial applicability (IA)

Yes: Claims

1-18

No: Claims

2. Citations and explanations (Rule 70.7):

see separate sheet

PCT/EP2004/009684

Re Item V

Reasoned statement with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

1). State of the art

Reference is made to the following documents dealing with a process for recycling expanded polystyrene by dissolving in a solvent and precipitating with a non-solvent.

D2: solvent may be diethyl carbonate; non-solvent is a lower alcohol.

D4: solvents are ethers or esters; non-solvent is a lower alcohol.

These differences establish novelty for independent process claim 1 (Art. 33(2) PCT).

2). Art. 33(1)(3) PCT - Inventive step

The distinguishing feature of claim 1 with regard to closest prior art D2 is that the non-solvent contains an alkylene carbonate. The technical effect is that this non-flammable compound allows a more efficacious removal of bromine compounds with respect to the use of alcohols alone (compare example 20 with example 22). The problem to be solved is to provide a process showing this effect in view of D2.

The solution of using alkylene carbonate non-solvents has not been mentioned in the state of the art, be it that in accordance with D4, the ester or ether solvents may comprise an amount of alkylene carbonate. The non-solvent, however, is an alcohol.

The skilled one will not contemplate to combine the teachings of D2 and D4, and arrive in this way to the process of claim 1.

Consequently, claim 1 is also based on an inventive step and the requirements of Art. 33(1) PCT are met.

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CLAIMS

- 1. A process for recycling expanded polystyrene comprising:
 - (a) volume reduction of expanded polystyrene by dissolution with

a dialkyl carbonate, or a blend of dialkyl carbonates, having the general formula (I):

- wherein R_1 and R_2 , the same or different, have the following meaning:
 - R_1 , R_2 represent linear, branched or cyclic alkyl radicals, containing from 1 to 12 carbon atoms, and the sum of the carbon atoms of R_1 and R_2 is between 2 and 15,
 - (b) removal of the insoluble components;
 - (c) selective precipitation of polystyrene with a non-solvent or a blend of non-solvents for polystyrene;
- (d) separation, drying and extrusion of the precipitated polystyrene, said process being characterised in that the selective precipitation of polystyrene is carried out with a non-solvent selected from alkylene carbonate or a blend consisting of an alcohol and an alkylene carbonate.

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<u>CLAIMS</u>

bonates, having the general formula (I):

O II R₁ O—C —O R₂

wherein R_1 and R_2 , the same or different, have the following meaning

- R_1 , R_2 represent linear, branched or cyclic alkyl radicals, containing from 1 to 12 carbon atoms, and the sum of the carbon atoms of R_1 and R_2 is between 2 and 15,

as solvents for expanded polystyrene. A Process

- 2. The use of a dialkyl carbonate, or a blend of dialkyl carbonates, according to claim 1, wherein:
- R_1 , R_2 represent linear or branched alkyl radicals, containing from 1 to 8 carbon atoms, and the sum of the carbon atoms of R_1 and R_2 is between 5 and 10.
- 3. The use of a dialkyl carbonate, or a blend of dialkyl carbonates, according to claim 2, wherein the dialkyl carbonates are selected from those having a flash point higher than 55°C.
 - 4. The use of dialkyl carbonate, or a blend of dialkyl carbonates, according to claim 3, wherein the dialkyl carbonates are selected from the group consisting of di-n-butyl carbonate, di-isobutyl carbonate, di-n-

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propyl carbonate.

A process for recycling expanded polystyrene compris-

- (a) volume reduction of expanded polystyreme by dissolution with a dialkyl carbonate, or a blend of dialkyl carbonates having formula (I);
- (b) removal of the insoluble components;
- (c) selective precipitation of polystyrene with a non-solvent or a blend of non-solvents for polystyrene;
- (d) separation, drying and extrusion of the precipitated polystyrene.
- ing to claim B, wherein, in step (a), the concentration of polystyrene in the solution is between 5 and 50% weight and the dissolution of the expanded polystyrene with dialkyl carbonate is carried out at atmospheric pressure, at a temperature ranging from 20 to 70°C.
- The process for recycling expanded polystyrene according to claim 8, wherein the concentration of polystyrene in the solution ranges from 15 to 40% by weight.

 The process for recycling expanded polystyrene accord-
- ing to claim %, wherein the dissolution of expanded

 polystyrene with dialkyl carbonate is effected in an

apparatus equipped with a stirring system and at room temperature.

- The process for recycling expanded polystyrene according to claim \$\mathcal{S}\$, wherein the selective precipitation of polystyrene in step (c) is effected by feeding the styrene solution to the non-solvent, or blend of non-solvents, maintained under turbulent stirring, onto the bottom of the precipitation reactor, below the stirring system.
- ing to claim , wherein the selective precipitation of polystyrene in step (c) is effected with a non solvent, selected from the group consisting of gly-cols, alcohols, alkylene carbonates, dialkyl carbonates with a number of carbon atoms equal to or higher than 17, alkyl esters of fatty acids.
 - ing to claim \$\mathcal{S}\$, wherein the quantity of non-solvent, or blend of non-solvents, used for selectively precipitating the expanded polystyrene in step (c) is in a weight ratio with the dialkyl carbonate of between 2:1 and 20:1.
 - The process for recycling expanded polystyrene according to claim 11, wherein the quantity of non-solvent, or blend of non-solvents, used is in a weight ratio

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- with the dialkyl carbonate of between 3:1 and 15:1.
- 18. The process for recycling expanded polystyrene according to claim \$\beta\$, wherein the selective precipitation of polystyrene in step (c) is effected at a temperature ranging from 10 to 70°C.
- 14. The process for recycling expanded polystyrene according to claim 13, wherein the selective precipitation is effected at a temperature ranging from 15°C to 60°C.
- ing to claim %, wherein the selective precipitation of polystyrene is effected by feeding the polystyrene solution to the non-solvent onto the bottom of the precipitation reactor, with a flow rate, expressed as g/(hour*liter of non-solvent), within the range of 30-1500.
 - The process for recycling expanded polystyrene according to claim 13, wherein the solution of polystyrene is fed to the non-solvent with a flow rate, expressed as g/(hour*liter of non-solvent), within the range of 50-800.
 - The process for recycling expanded polystyrene according to claim 8, wherein the separation of polystyrene precipitated in step (d) is effected by filtration, decanting, centrifugation, at a temperature ranging

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from 10°C to 70°C.

- The process for recycling expanded polystyrene according to claim 1/1, wherein the separation of the precipitated polystyrene is effected at a temperature within the range of 15°C 60°C
- The process for recycling expanded polystyrene according to claim 5, wherein the drying of the polystyrene precipitated in step (d) is effected at a temperature ranging from 50°C to 180°C and a pressure of between 760 and 1 mm Hg.
- ing to claim 19, wherein the drying is effected at a temperature ranging from 80°C to 150°C and a pressure of between 500 and 10 mm Hg.

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